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**Amendments to the Claims:** This listing of claims will replace all prior versions, and listings, of claims in the application. Claim 1 was amended to incorporate the limitations of claim 2. Claim 2 was cancelled. Claims 26-49 are new. Support for the new claims is found at page 4, line 6; page 5, line 1 and the Examples. No new matter has been added.

**Listing of Claims:**

- 1                   1. (Currently Amended) A process of treating internal  
2                   combustion engine exhaust gas containing O<sub>2</sub>, NO<sub>x</sub>, unburnt hydrocarbon  
3                   ("HC"), CO and soot, comprising:]  
4                   i. catalytically oxidizing a substantial part of the HC;  
5                   ii. catalytically treating the product of step i to oxidize NO  
6                   to NO<sub>2</sub>;  
7                   iii. collecting soot; and  
8                   iv. combusting the collected soot by reaction with the NO<sub>2</sub>  
9                   and possibly any O<sub>2</sub> left over after steps i and ii.  
1                   2. (Cancelled)  
1                   3. (Previously Presented) Process according to claim 1  
2                   carried out over:  
3                   i. a first catalyst adapted to be fed with engine exhaust  
4                   gas and effective to promote oxidation of HC therein;  
5                   ii. a second catalyst adapted to be fed with the product of i  
6                   and effective to promote oxidation of NO to NO<sub>2</sub>;  
7                   iii. a filter effective to collect soot and to retain it until  
8                   combusted by said NO<sub>2</sub> and any O<sub>2</sub> left over after catalyst i and ii;  
1                   4. (Original) Process according to claim 3 in which the  
2                   catalysts are honeycomb-supported.  
1                   5. (Original) Process according to claim 4 in which the cell  
2                   density of the honeycomb is in the range 100-900 per square inch.  
1                   6. (Previously Presented) Process according to claim 1 in  
2                   which the gas leaving step/catalyst i undergoes cooling and then enters  
3                   step/catalyst ii.  
1                   7. (Original) Process according to claim 6 in which the first  
2                   oxidation is carried out close to the source of exhaust gas, whereby to obtain  
3                   a maximum convenient operating temperature and reaction rate.

1                   8. (Previously Presented) Process according to claim 6 in  
2                   which the gas leaving step/catalyst i undergoes cooling and then enters  
3                   step/catalyst ii.

1                   9. (Previously Presented) Process according to claim 6,  
2                   further comprising providing an increased amount of combustible upstream of  
3                   a first catalyst for effecting step i for increasing the temperature at which step  
4                   i operates.

5                   10. (Original) Process according to claim 9 in which said  
6                   combustible is provided by modifying engine settings to pass more HC and/or  
7                   generate more CO.

1                   11. (Previously Presented) Process according to claim 6 in  
2                   which a first catalyst for effecting step i has a very low light-off temperature  
3                   for HC and CO oxidation.

1                   12. (Previously Presented) Process according to claim 1,  
2                   wherein the HC is absorbed on the soot.

1                   13. (Previously Presented) Process according to claim 1,  
2                   further comprising removing NOx downstream of soot combustion.

1                   14. (Previously Presented) Process according to claim 13  
2                   wherein removing NOx uses a regenerable NOx absorber downstream of the  
3                   collecting trap.

1                   15. (Original) Process according to claim 14 including  
2                   catalytic NOx-removal downstream of the NOx absorber.

1                   16. (Previously Presented) System for treating internal  
2                   combustion engine gas containing O<sub>2</sub> NOx, unburnt hydrocarbon ("HC"), CO  
3                   and soot, comprising:

4                   i.           a first catalyst to receive engine exhaust and effective to  
5                   promote oxidation of HC therein;

6                   ii.          a second catalyst receiving the product of the first  
7                   catalyst and effective to promote oxidation of NO to NO<sub>2</sub>; and

8                   iii.        a filter effective to collect soot and to retain it until  
9                   combusted by reaction with said NO<sub>2</sub> and, depending on conditions, any O<sub>2</sub>  
10                  left over after the first catalyst.

1                   17. (Original) System according to claim 16 in which the  
2                   catalysts are honeycomb-supported.

1                   18. (Original) System according to claim 17 in which the  
2                   cell density of the honeycomb is in the range 100-900 per square inch.

1                   19. (Previously Presented) A diesel engine in combination  
2                   with a system according to claim 16 connected to its exhaust.

1               20. (Original) An engine according to claim 19 which is one  
2               designed for light duty applications.

1               21. (Original) An engine according to claim 20 which is of  
2               the turbo-charged direct injection type.

1               22. (Original) An engine combination according to claim 19,  
2               which is a heavy duty engine.

1               23. (Original) An engine combination according to claim 22,  
2               wherein the first catalyst is positioned close to the second catalyst.

1               24. (Original) An engine combination according to claim 23,  
2               wherein the first catalyst and the second catalyst are at opposite ends of a  
3               single catalyst monolith.

1               25. (Previously Presented) Process according to claim 1  
2               wherein step i further comprises oxidizing some NO to NO<sub>2</sub>.

1               26. (New) A process according to claim 1, wherein the first  
2               catalyst comprises at least one supported platinum group metal (PGM).

1               27. (New) A process according to claim 26, wherein the at  
2               least one supported PGM is selected from the group consisting of platinum,  
3               palladium and rhodium.

1               28. (New) A process according to claim 27, wherein the at  
2               least one PGM is platinum and palladium.

1               29. (New) A process according to claim 27, wherein the  
2               support is selected from the group consisting of alumina, ceria and alumina  
3               and ceria.

1               30. (New) A process according to claim 28, wherein the  
2               support is selected from the group consisting of alumina, ceria and alumina  
3               and ceria.

1               31. (New) A process according to claim 27 comprising a  
2               first layer comprising platinum-catalyzed alumina and a second layer  
3               comprising ceria overlying the first layer.

1               32. (New) A process according to claim 27, comprising from  
2               10-150g/ft<sup>3</sup> platinum.

1               33. (New) A process according to claim 1, wherein the  
2               second catalyst comprises at least one supported platinum group metal  
3               (PGM).

1               34. (New) A process according to claim 33, wherein the at  
2               least one supported PGM is selected from the group consisting of platinum,  
3               palladium and rhodium.

1               35. (New) A process according to claim 34, wherein the at  
2               least one PGM is platinum.

1               36. (New) A process according to claim 35, wherein the  
2               support is alumina.

1               37. (New) A process according to claim 35, comprising from  
2               10-150g/ft<sup>3</sup> platinum.

1               38. (New) A system according to claim 16, wherein the first  
2               catalyst comprises at least one supported platinum group metal (PGM).

1               39. (New) A system according to claim 38, wherein the at  
2               least one supported PGM is selected from the group consisting of platinum,  
3               palladium and rhodium.

1               40. (New) A system according to claim 39, wherein the at  
2               least one PGM is platinum and palladium.

1               41. (New) A system according to claim 39, wherein the  
2               support is selected from the group consisting of alumina, ceria and alumina  
3               and ceria.

1               42. (New) A system according to claim 40, wherein the  
2               support is selected from the group consisting of alumina, ceria and alumina  
3               and ceria.

1               43. (New) A system according to claim 39 comprising a first  
2               layer comprising platinum-catalyzed alumina and a second layer comprising  
3               ceria overlying the first layer.

1               44. (New) A system according to claim 39, comprising from  
2               10-150g/ft<sup>3</sup> platinum.

1               45. (New) A system according to claim 16, wherein the  
2               second catalyst comprises at least one supported platinum group metal  
3               (PGM).

1               46. (New) A system according to claim 45, wherein the at  
2               least one supported PGM is selected from the group consisting of platinum,  
3               palladium and rhodium.

1               47. (New) A system according to claim 46, wherein the at  
2               least one PGM is platinum.

1               48. (New) A system according to claim 47, wherein the  
2               support is alumina.

1               49. (New) A system according to claim 47, comprising from  
2               10-150g/ft<sup>3</sup> platinum.